

## IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Patent Application of  
TAKESHI MATSUMOTO ET AL

5    Serial No. 10/535,511                      Group Art Unit: 1755  
    Filed: May 18, 2005                      Examiner: Wood, Elizabeth D  
    Title: EXHAUST GAS PURIFYING CATALYST AND PROCESS FOR  
    PURIFYING EXHAUST OF GAS

10

DECLARATION  
UNDER 37 C.F.R. 1.132

    Being duly sworn, I, Takuji Nakane, a citizen of Japan,  
15    residing at 344-1-706, Waku, Aboshi-ku, Himeji-shi, Hyogo-ken,  
    Japan, depose and say:

    I. I am one of co-inventors in the above referenced  
    application, and a chemist as well as a Researcher of AC  
    Research Laboratory of ICT CO., LTD., one of co-assignees  
20    of this application, on the subject matters relating to this  
    application.

    I graduated from Tokyo Institute of Technology, Faculty  
    of Science, Department of Chemistry in March 1997 and Graduate  
    School of Tokyo Institute of Technology, Department of  
25    Chemistry in March 1999, and obtained a master degree majoring  
    chemistry.

    From April, 1999 up till the present, I have been the  
    employee of ICT CO., LTD. at AC Research Laboratory of this  
    company, I have been engaged in the research work with respect  
30    to catalysts for purifying exhaust gas of diesel engine.

    I am well acquainted with all of the co-inventors in  
    this case, having worked with them on the development thereof,

well as my own.

II. In order to compare the effects of the catalysts of the  
5 above-identified Matsumoto et al application Serial No.  
10/535,511 with those catalysts of JP07-289910, JP05-220403  
and EP 0415410, I made the experiments as follows:

#### Example 6

10 A similar method to Example 1 of Matsumoto et al (USSN  
10/535,511) is carried out except that, 211g of ZSM5 and 43g  
of  $\beta$ -zeolite (same as in Example 5 of Matsumoto et al (USSN  
10/535,511)) are used instead of 250g of ZSM5. The catalyst  
thus obtained was supported 7g of copper oxide (CuO), 80g  
15 of ZSM5, 15g of  $\beta$ -zeolite and 3g of magnesium oxide (MgO)  
per liter of the carrier.

#### Example 7

The catalysts obtained in Example 1, 5 and 6 thus obtained  
20 were subjected to experiments by a similar method of Examples  
at a catalyst inlet temperature of 500°C to obtain NOx  
conversion and SO<sub>2</sub> conversion. In such case, the exhaust  
gas compositions before addition of the light oil were 380ppm  
of NOx, 60ppm of HC, 100ppm carbon dioxide and 10ppm of SO<sub>2</sub>.  
25 The results are shown in Table 3.

Then, under maintaining the 2,200rpm of rotation number  
of the engine, open degree of the throttle of the engine was  
controlled, and a catalyst inlet temperature was decreased  
to 350°C to be stable, and then the exhaust gas before addition  
30 of the light oil was measured by a similar method at 500°C  
(Table 4). In such case, the exhaust gas composition before  
addition of light oil were 270ppm of NOx, 80ppm of HC, 100ppm

of carbon monoxide and 7ppm of SO<sub>2</sub> (Table 5).

In the condition at 350°C, light oil as a reducing agent for NO<sub>x</sub> was supplied at a position of upper stream side from the catalyst layer in a rate of 5.5 ml/min. In such case,  
5 the results were shown in Table 6.

Table 3

	CuO	ZSM5 (MFI type zeolite)	BEA (β zeolite)	ZSM5:BEA	Others
		H type SiO <sub>2</sub> /Al <sub>2</sub> O <sub>3</sub> =80	NH <sub>4</sub> type SiO <sub>2</sub> /Al <sub>2</sub> O <sub>3</sub> =25		
		Average crystal diameter < 0.05 μm			
Example 1	7	95		1:0	Mg 3 (as oxide)
Example 2	7	95		1:0	Mg 1 (as oxide)
Example 3	7	95		1:0	Mg 5 (as oxide)
Example 4	7	95		1:0	Ca 3 (as oxide)
Example 5	7	70	25	14:5	Mg 3 (as oxide)
Example 6	7	80	15	16:3	Mg 3 (as oxide)
Control 1	7	95		1:0	

Table 4 (at 500°C)

	NO <sub>x</sub> conversion	SO <sub>2</sub> conversion
Example 1	18	22
Example 2	16	41
Example 3	16	15
Example 4	16	33
Example 5	17	24
Control 1	16	60

10

Table 5 (at 500°C)

	NO <sub>x</sub> conversion	SO <sub>2</sub> conversion
Example 1	17	14
Example 5	17	17
Example 6	16	15

Table 6 (at 350°C)

	NOx conversion	SO <sub>2</sub> conversion
Example 1	14	0
Example 5	23	0
Example 6	20	1

### III. CONCLUSION

As being clear from the above-mentioned examples, the  
5 effect of a mixture of ZSM5 with  $\beta$ -zeolite in a specific ratios  
resides in widen the windows of NOx conversion.

The undersigned Takuji Nakane declared that all the  
statements made herein are true; and further that these  
statements were made with the knowledge that willful false  
10 statements and the like so made are punishable by fine or  
imprisonment, or both under Section 1001 of Title 18 of the  
United States Code and that such willful false statements  
may jeopardized the validity of the application or any patent  
issuing thereon.

15

Dated this 18th day of September, 2007.

By Takuji Nakane  
Takuji Nakane

20